

Effect of Lewis Number on Double-diffusive Natural Convection in a Triangular Cavity

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ABSTRACT

This paper concerned with the numerical study of thermal and mass diffusive natural convection flow inside a triangular shape solar collector using finite element method for the governing equations expressing the velocity pressure formulation along with the energy and concentration balance equations. In the solution procedure, the isothermal and iso-concentration boundary conditions are assumed at the absorber and covers of collector. Local and mean heat and mass transfer rates for the thermal Rayleigh number and Lewis number are presented. Streamlines, isotherms and iso-concentration are also presented for the aforesaid parameters. The result found in this study fully agreed with the previous published work. But this result will be profitable for the design of the collector.

Keywords

Solar collector; natural convection; finite element method; absorber.

1. INTRODUCTION

Finite element method techniques are widely used in problems of consisting of complex geometry and partial differential equations. In this method of analysis, the considered domain is discretized into simple geometric shapes called finite elements. The materials property and the governing relationships are considered over these elements and expressed in terms of unknown values at element corner. An assembly process duly considering the loading and constraints, results in a set of equations. Solution of these equations gives us the approximate behavior of the continuum. Thompson [1] discusses solution of partial differential equations involved in areas such as Fluid Mechanics, Elasticity and Electromagnetic Field by using FEM. Details about fluid mechanics and heat transfer problems and their solution can be found in [2]. A more complex transient heat conduction equation is discussed in Winget and Hughes [3].

Natural convection flow and heat transfer in different geometrical enclosures such as triangular, square, rectangular and trapezoidal enclosures etc. which are the main piece of solar energy system, have been the topic of many research engineering studies. These studies consist of various technological applications such as solar collectors, building heating and ventilation, cooling electronically devices [4-6]. Double-diffusive natural convection occurs within the solar

collector, owing to the collective thermal and mass diffusion buoyancy effects as well as the temperature difference between cover and absorber. Nowadays, the study of solar collectors is one of the most significant works to progress their performance with a competitive price [7]. Numerical solution has the advantage over an experimental investigation in that the important parameters, such as geometrical dimensions, glass thickness and covenant location may be simply changed. Therefore, its persuading on the overall heat and mass transfer can be studied at a low price. Numerical investigation is also helpful in testing the performance of solar collectors for different components.

Several experiments and theoretical investigations have been undertaken in this region. Boukar and Harmim [8] experimentally investigated design parameters of an indirect vertical solar still. Omri et al. [9] examined the thermal exchange by natural convection and effect of buoyancy force on flow structure. The authors provided useful information on the flow structure sensitivity to the governing parameters, the Rayleigh number and the tilt angle on the thermal exchange. Omri [10] numerically studied the flow characteristics inside an asymmetrical triangular still for the configuration optimization. Gao et al. [11] performed a study on natural convection inside the wavy and inclined solar collectors, but they did not consider flow behavior and thermal fields. A numerical experiment is performed for inclined solar collectors by Varol and Oztop [12].

Different types of solar still available in the literature are conventional solar stills, single-slope solar still with passive condenser, double condensing chamber solar still [13], vertical solar still [14], the inverted absorbers solar still [15] and multiple effect solar still [16]. The heat transfer inside the isosceles triangular enclosure is studied by Varol et al. [17-19] for different thermal boundary conditions, including entropy generation. Double-diffusive natural convection inside an isosceles triangular solar collector was discussed by Rahman et al. [7]. In their study, the considered fluid inside the cavity was air with $Pr = 0.71$ and taking Lewis number was fixed at $Le = 2.0$. In this paper, natural convection heat and mass transfer in a triangular shaped enclosure for different Lewis and Rayleigh number are thoroughly studied.

Nomenclature			
B_r	buoyancy ratio	T_h	hot wall temperature (source)
C	concentration of species	T_L	cold wall temperature (sink)
C_h	high species concentration (source)	u, v	dimensional velocity components
C_L	high species concentration (sink)	U, V	dimensionless velocity components
C^*	dimensionless species concentration	x, y	dimensional coordinates
D	species diffusivity	X, Y	dimensionless coordinates
G	gravitational acceleration	<i>Greek symbols</i>	
H	enclosure height	A	thermal diffusivity (m^2s^{-1})
Le	Lewis number	B_T	thermal expansion coefficient
Nu	Nusselt number	β_c	compositional expansion coefficient
P	dimensional pressure (Nm^{-2})	M	dynamic viscosity ($Kg\ m^{-1}s^{-1}$)
P	non-dimensional pressure	N	kinematic viscosity (m^2s^{-1})
Pr	Prandtl number	θ	non-dimensional temperature
Ra	Rayleigh number	ρ	Density
Sh	average Sherwood number	Ψ	Stream function
T	temperature (K)	Γ	general dependent variable

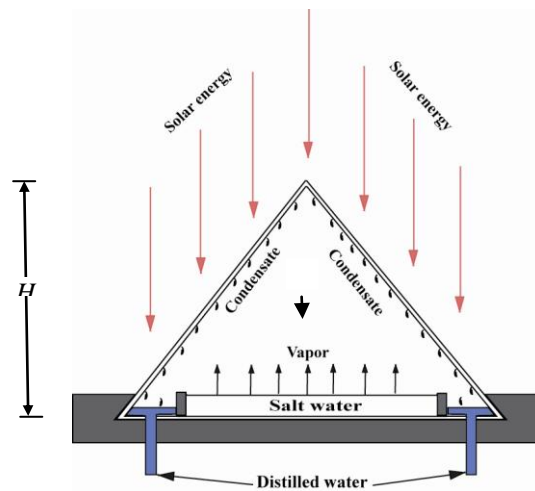


Fig. 1. Schematic diagram for the problem

2. PROBLEM STATEMENT

2.1 Physical description

The physical phenomenon of the considered domain is shown below. A triangular shaped solar collector is considered here. The enclosed space consists mostly of an absorber plate and two inclined glass covers that form a cavity. The absorber plate is represented by a horizontal bottom wall kept to a constant temperature T_h while the inclined walls are considered transparent and maintained at a constant temperature T_L with $T_h > T_L$.

2.2 Mathematical formulation

The governing equations for the problem under consideration are based on the balance laws of mass, momentum and

thermal energy in two dimensions. Following the previous assumptions, these equations can be written in non-dimensional form as:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0 \quad (1)$$

$$U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} = -\frac{\partial P}{\partial X} + Pr \left(\frac{\partial^2 U}{\partial X^2} + \frac{\partial^2 U}{\partial Y^2} \right) \quad (2)$$

$$U \frac{\partial V}{\partial X} + V \frac{\partial V}{\partial Y} = -\frac{\partial P}{\partial Y} + Pr \left(\frac{\partial^2 V}{\partial X^2} + \frac{\partial^2 V}{\partial Y^2} \right) + Ra_T Pr (\theta + BrC) \quad (3)$$

$$U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} = \frac{\partial^2 \theta}{\partial X^2} + \frac{\partial^2 \theta}{\partial Y^2} \quad (4)$$

$$U \frac{\partial C}{\partial X} + V \frac{\partial C}{\partial Y} = \frac{1}{Le} \left(\frac{\partial^2 C}{\partial X^2} + \frac{\partial^2 C}{\partial Y^2} \right) \quad (5)$$

where the dimensionless variables are introduced as:

$$X = \frac{x}{H}, Y = \frac{y}{H}, U = \frac{uH}{\nu}, V = \frac{vH}{\nu}, P = \frac{(\rho + \rho_0 y)H^2}{\rho\nu^2}, \theta = \frac{T - T_L}{T_h - T_L}, C = \frac{c - c_L}{c_h - c_L} \quad (6)$$

The variables have their usual sense in fluid mechanics and heat transfer as listed in the nomenclature. It can be seen from the Eqs. (2) - (5), five parameters that preside over this problem are the Prandtl number (Pr), the thermal Rayleigh number (Ra_T), Lewis number (Le) and buoyancy ratio (Br), which are defined respectively as

$$Pr = \frac{\nu}{\alpha}, Ra_T = \frac{g\beta_T(T_h - T_L)H^3}{\alpha\nu}, Le = \frac{\alpha}{D}, Br = \frac{\beta_c(c_h - c_L)}{\beta_T(T_h - T_L)} \quad (7)$$

The dimensionless boundary conditions corresponding to the considered problem are as follows

on the bottom wall: $U = V = 0, \theta = C = 1$

on the inclined walls: $U = V = 0, \theta = C = 0$

The local heat and mass transfer rates on the surface of heat and contaminant sources are defined respectively as

$$Nu = -\left(\frac{\partial\theta}{\partial Y}\right)_{Y=0} \quad \text{and} \quad Sh_x = -\left(\frac{\partial C}{\partial Y}\right)_{Y=0}$$

The average heat and mass transfer rates on the surface of heat and contaminant sources can be evaluated by the average Nusselt and Sherwood numbers, which are defined respectively as

$$Nu = -\int_0^1 \frac{\partial\theta}{\partial Y} dX \quad (8)$$

$$\text{and} \quad Sh = -\int_0^1 \frac{\partial C}{\partial Y} dX \quad (9)$$

The stream function is calculated from

$$U = \frac{\partial\psi}{\partial Y}, V = -\frac{\partial\psi}{\partial X} \quad (10)$$

3. NUMERICAL SOLUTION

3.1 Solution procedure

The Gelarkin weighted residual technique of finite element method is used in this task. In the finite element method, the region of interest can be discretized using different types of element shapes and sizes, called elements. The dependent variables are then approximate over these elements. In this study, the triangular element is considered. Using FEM, the governing Eqs (2-5) are transferred into a set of algebraic equations. The system of algebraic equations is solved using iterative method. The iterative process is continuing until the

following convergence condition is satisfied: $|\Gamma^{i+1} - \Gamma^i| \leq 10^{-6}$ where i is the number of iteration and Γ is the general dependent variable.

3.2 Grid refinement checks and code validation

In FEM solution procedure, the accuracy of the numerical result can be enhanced by using either higher order elements or increasing the number of elements. The number of elements is increased to get the desired accuracy as well as to get the grid independent solution of this study. A trial calculation is made using various non-uniform grids of triangular elements: 1486, 3396, 4590 and 5112 in order to obtain the desired grid independent solutions. The calculation of average Nusselt number and Sherwood numbers are carried

out using $Ra_T = 10^6$, $Pr = 0.71$ and $Br = 10.0$ for these five non-uniform grid. Finally, the grid size of about 3396 elements was chosen through this study for the balance between the calculation accuracy and the speed. The study is compared with an earlier work performed by Kent et al. [20] and found a good agreement which ensure the code validation of this analysis. The comparison result is shown in fig-2.

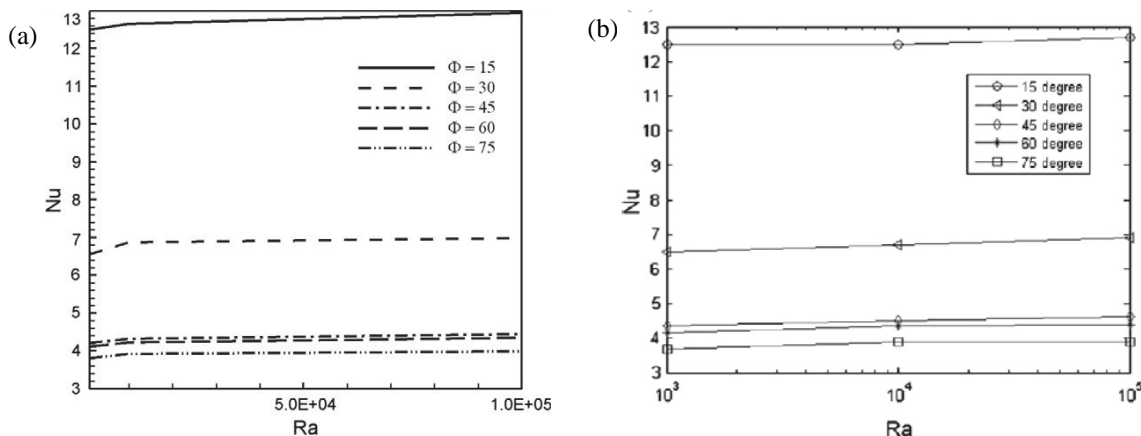


Fig-2. Comparison of the (a) present model with (b) the results of Kent [20] for natural convection inside a isosceles triangular enclosure for five different base angles.

4. RESULTS AND DISCUSSION

A computational analysis has been performed to investigate the effects of Lewis number on natural convection inside an isosceles triangular solar collector using Gelarkin weighted residual finite element technique. Air was used inside the cavity as a working fluid with $Pr = 0.71$. The effective

parameters are buoyancy ratio, Rayleigh number, Lewis number etc. The buoyancy ratio and Rayleigh number were considered fixed at $Br=10$ and $Ra = 10^6$ throughout this analysis. Fig-3 demonstrates the effect of Lewis number on streamline, isotherm and iso-concentration. As seen from the figures, symmetric flow distribution is observed inside the cavity according to the middle axis of the triangle. In the case

of stream lines for low Lewis number, the number of circular cell trends to increase. But due to the increase of Lewis number from 1.0 to 10.0, there are only two circular cells inside enclosure and the strength of flow increases. The left cell rotates counterclockwise while the right cell rotates clockwise. In the case of temperature distribution, convective distortion of the isotherms occurs throughout the cavity due to the strong influence of the convective current in the cavity. It is evident that flow of the temperature increases with increase

of Lewis number. A similar distribution of iso-concentration exhibits with increase of Lewis number.

Fig-4 illustrates the average heat transfer rate with the increase of Lewis and Rayleigh number. Average heat transfer increases from 0.1 to 1.0 and shows decreasing trends from 1.0 to 10 with increase of Lewis and Rayleigh number. But in the case of average mass transfer, it exhibits speedily increases with increase of Lewis and Rayleigh number which shows in fig-5.

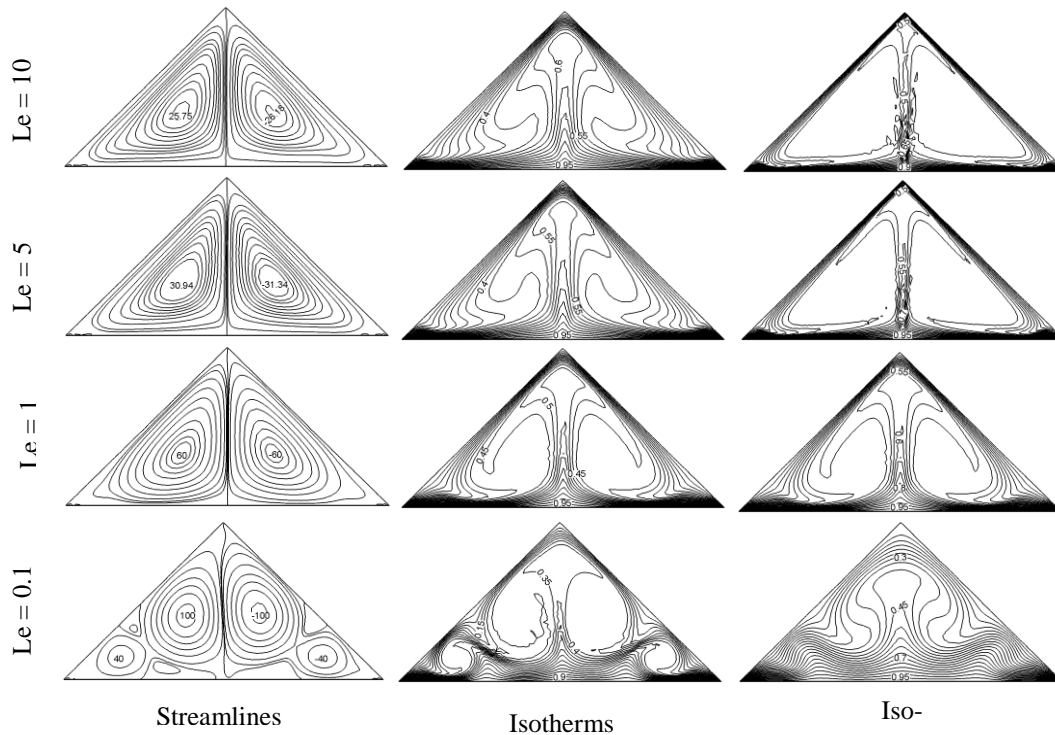


Fig. 3. Effect of Lewis number on streamlines, isotherms and iso-concentration, while $Ra = 10^5$

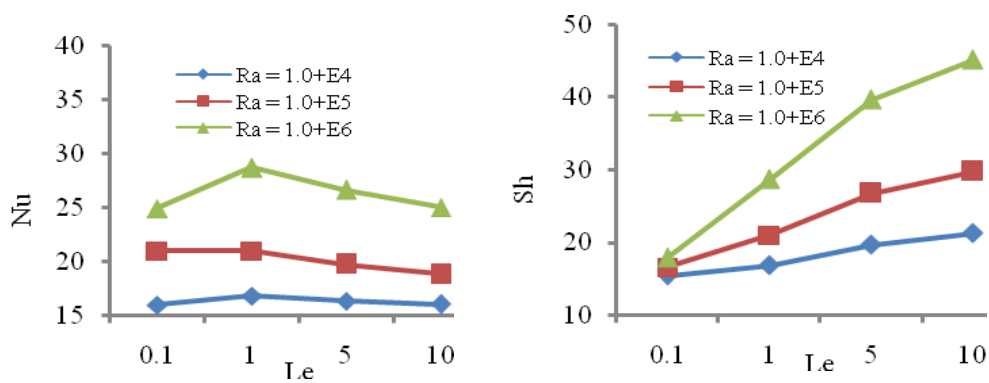


Fig-4 Effect of Lewis number on average Nusselt number (Nu) and average Sherwood number (Sh)

5. CONCLUSIONS

This numerical study concerned with the fluid flow, heat transfer and mass transfer inside triangular shaped solar collectors. The results are obtained for different values of Lewis and Rayleigh numbers. It is observed that mass transfer increases with increase of Lewis and Rayleigh numbers and formed symmetric flow field, temperature distribution and

mass distribution according to the middle axis of the triangular cavity. But the heat transfer at first increases and then decreases with the increases of Lewis and Rayleigh numbers and formed symmetric flow field, temperature distribution and mass distribution according to the middle axis of the triangular cavity.

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